



(12) **EUROPEAN PATENT APPLICATION**

(43) Date of publication:
08.09.2004 Bulletin 2004/37

(21) Application number: **03004726.0**

(22) Date of filing: **04.03.2003**

(51) Int Cl.7: **A61L 2/07, A61K 31/56,
A61K 31/57, A61K 31/573,
C07J 5/00, C07J 7/00,
C07J 51/00, C07J 75/00**

(84) Designated Contracting States:
**AT BE BG CH CY CZ DE DK EE ES FI FR GB GR
HU IE IT LI LU MC NL PT SE SI SK TR**
Designated Extension States:
AL LT LV MK RO

(71) Applicant: **Dompé S.P.A.**
I-67100 L'Aquila (IT)

(72) Inventors:
• **Gentile, M. Marco**
67100 L'Aquila (IT)

• **Dell'Uomo, Marco**
67100 L'Aquila (IT)
• **Dragani, M. Concetta**
67100 L'Aquila (IT)

(74) Representative: **Pieraccioli, Daniele**
Dompé S.p.A.,
Via San Martino, 12
20122 Milano (IT)

(54) **Sterilization of glucocorticoid drug particles for pulmonary delivery**

(57) A process for the sterilization of water insoluble solid medicinal substances is described. The process provides the sterilization of drug substances, which are suitable for pulmonary administration. In particular, the process is used in industrial plants for the production of formulation of sterile glucocorticoids for inhalation delivery, so as to avoid any modifications in particle size distribution and in the impurities profile of the drug. The

process is carried out by heating a mixture of micronized glucocorticoid and purified water only, preferably at a temperature of about 120° C for 20 minutes. The process is particularly efficient and economic for the steam sterilization of beclomethasone dipropionate in formulations for pulmonary delivery.

Description**Brief description of the invention**

5 [0001] The present invention relates to a process for the sterilization of water insoluble solid medicinal substances in aqueous suspensions, which are suitable for pulmonary administration. In particular, the invention relates to the steam sterilization of glucocorticoids, such as beclomethasone dipropionate, for inhalation delivery.

Background of the invention

10

[0002] The process for sterilizing powdered forms of water insoluble drug substance to be suspended into a sterile aqueous vehicle suitable for the pulmonary administration, such as non-electrolyte corticosteroids, glucocorticoids and the like, is still a critical process. The major problems are related to the high temperatures of the sterilization process and to the consequent thermal instability of the drug substance that frequently leads to degradation with modification

15

of the impurities profile and of the physico-chemical characteristics of the drug.
[0003] For solid drug substances suitable for inhalation delivery to be suspended in aqueous formulations, the particle size distribution, as well as its preservation during the shelf-life of the finished product, are particularly crucial parameters.

20

[0004] The particle size influences, in fact, the distribution of the drug into the lung and, as a consequence, the activity and effectiveness of the drug itself. It is generally accepted that the mean diameter of the particles in a formulation for inhalation delivery must be less than 10 microns, preferably about 5 microns or less.

[0005] Solid non-electrolyte corticosteroids, steroids as well as non-steroid drugs for use in aqueous suspensions are usually sterilized in different ways, for example by exposure to gases, or by aseptic crystallisation, drug heat sterilization, or by β and γ irradiation.

25

[0006] The sterilizing treatment can cause adverse physical and chemical changes of the drug substance and all parameters have to be checked and investigated in the preliminary phase of the process development.

[0007] In the case of drug substances intended for inhalation use, in addition to the control of the physical and chemical stability of the sterilized drug, it is then crucial to prevent any unacceptable change in particle size due to possible recrystallization of the drug, which is consequent to many known sterilization methods.

30

[0008] A process for the steam sterilization of solid non-electrolyte corticosteroids is described by O'Neill in US 3,962,430. The process is carried out in a saturated sodium chloride solution at the sterilizing temperature. Sodium chloride is reported to be necessary to prevent recrystallization of the solid particles and any possible change in crystal size or form of the corticosteroid upon re-cooling.

35

[0009] WO 00/25746 describes a process for the preparation of suspensions of drug particles for inhalation delivery and includes sterilization with gamma irradiation, stating that beclomethasone dipropionate suspensions subjected to wet steam process, under conditions similar to those reported in US 3,962,430 (121°C for 15 minutes), undergo a remarkable decrease in the content of the active ingredient with a significant increase in degradation products (about 10-11 %).

40

[0010] Steam sterilization of the aqueous suspensions of glucocorticoids is also reported by Karlsson (WO 99/25359) to lead to unacceptable changes in particle size. Karlsson makes reference to the wet steam method described by O'Neill in US 3,962,430 stating that such method is not suitable for suspensions of fine particles of glucocorticosteroids which are intended for inhalation because the water, and the heating and the cooling involved, produce unfavourable changes in the size of the particles.

45

[0011] In order to eliminate the problem of changes in particle size, Karlsson uses dry heat sterilization which is, anyway, known to be often unsuitable for solid drug compounds since it causes adverse physical and chemical changes such as discoloration and degradation of the solids even at temperatures below 120° C.

Description of the drawings

50

[0012]

Figure 1: Particle size distribution of the drug substance BDP batch 4 sterilised (S), not sterilised (NS) and sterilised in presence of NaCl 0.420 g/mL (S NaCl(B)) and of NaCl 0.570 g/mL (S NaCl(C)).

55

Figure 2: Particle size distribution of the drug substance BDP batch 5 sterilised (S), not sterilised (NS) and sterilised in presence of NaCl 0.420 g/mL (S NaCl(B)) and of NaCl 0.570 g/mL (S NaCl(C)).

Figure 3: Particle size distribution of formulation PG038/115 (BDP batch 4 sterilised) and PG038/119 (BDP batch 4 not sterilised) after 50 days of storage at 40°C 75%R.H.

Figure 4: Particle size distribution of formulation PG038/116 (S) (BDP batch 5 sterilised) and formulation

PG038/120 (NS) (BDP batch 5 not sterilised) after 50 days of storage at 40°C 75%R.H.

Detailed description of the invention

5 [0013] We have unexpectedly found, given the teachings of the prior art, a simple and economic process for the sterilization of solid medicinal substances, in particular of glucocorticoids, such as dexametasone, monomethasone, fluticasone, beclomethasone and their salts, using an aqueous suspension of the substance and avoiding the complex and more expensive processes of the prior art. The process of the present invention is particularly suitable for beclomethasone dipropionate (BDP) (Prontinal® - Dompé) and the use of said process in industrial plants allows an easier and less expensive manufacturing process. The sterilisation of the active ingredient can be performed directly in the preparation vessel (turbomogenizer working as an autoclave); in this way the bulk preparation and the transfer of bulk to the filling machine can be carried out without any contact with the environment (aseptic condition). As a consequence, qualification and controls of preparative area, personnel gowning and training as well as cleaning procedures, result to be less heavy in terms of costs and timing.

15 [0014] It is thus an object of the present invention to provide a process for the steam sterilisation of glucocorticoids, comprising heating a mixture of water and micronised glucocorticoid at a temperature ranging between 100° and 130°C for a time sufficient to sterilise the mixture with a minimum S.A.L. (Sterility Assurance Level) of 10^{-6} , the mixture being a mixture of glucocorticoid and water only. The micronised glucocorticoid:water (w:w) ratio can range between 2.5:100 and 100:2. When the ratio is 100:2 the mixture is intended to be a micronised hydrated glucocorticoid powder).

20 [0015] Preferably the glucocorticoid is beclomethasone and more preferably is beclomethasone dipropionate.

[0016] The micronised glucocorticoid:water ratio is preferably between 3:100 (about 30mg/mL) to 10:100 (about 100mg/mL).

[0017] Mixtures of the glucocorticoid and water at different ratios were prepared and the mixtures were steam sterilised at a temperature of about 120° C for a time ranging from 15 to 30 minutes.

25 [0018] Preferably steam sterilization was carried out at 121°C for 20 minutes.

[0019] The purity of BDP sterilised according to the present invention was compared with the purity of the starting, non-sterilised BDP.

[0020] The distribution in the particle size and the water stability of the sterilised BDP was also determined in order to verify the steam treatment effects on crystal growth.

30 [0021] In parallel, steam sterilization of BDP in the presence of saturated sodium chloride, according to US 3,962,430, was also carried out.

[0022] The amount of sodium chloride was in the range between 1.1 mg to 1.5 mg per 2.6 mg of water, according to the teachings of US 3,962,430. The comparative tests were then carried out with mixtures NaCl:BDP:water in the ratio 42:4:100 and 57:4:100, corresponding to an aqueous suspension containing about 40mg of BDP and 420mg or 570mg of sodium chloride in a final volume of 1mL.

35 [0023] The comparative steam sterilization in the presence of saturated sodium chloride was carried out at the same temperature and for the same time as the steam sterilization experiments carried out according to the present invention.

[0024] Stability studies were also performed with formulations suitable for inhalations prepared using the steam sterilised BDP suspensions of the present invention in comparison with formulations containing non-sterilized BPD.

40 [0025] Analyses for particle size and HPLC purity were performed on samples after 50 days of storage at 40° C, 75% R.H.

[0026] Results show that the impurities profile of the sterilised glucocorticoid suspensions of the present invention are not significantly different from the profile of the non-sterilised glucocorticoid.

45 [0027] Also the particle size distribution of the sterilised suspensions is not different from the particle size distribution of the non-sterilised glucocorticoid and is not different from the size of the glucocorticoid sterilised in a sodium chloride saturated solution. Sodium chloride does not affect the crystal size of aqueous beclomethasone dipropionate suspensions, contrary to what stated in the art by O'Neill (US 3,962,430).

50 [0028] In addition, no significant differences were found in crystal growth and size distribution between formulations prepared with steam sterilised glucocorticoid and with non-sterilised glucocorticoid, after storage under accelerated conditions, for 50 days at 40°C 75% R.H.

Data processing

55 [0029] The experimental data, obtained during analytical determination were processed by means of the statistical function of Analysette 22 program version 1.70.

HPLC purity of drug substance and drug product

[0030] The acceptance limits of impurities are defined in the monograph of the drug substances and drug product.
[0031] Impurities with content greater than 0.05% with reference to BDP content of the analysed sample are reported.
[0032] The HPLC purity of sterilised 4mg/mL and 40mg/mL aqueous BDP suspension were checked in comparison with non-sterilised BDP drug substance.
[0033] Synthesis drug substance impurities are not reported.
[0034] In table 1 the analytical data of three different batches of BDP drug substances (1, 2 and 3) steam sterilised at concentration of 4mg/mL and 40mg/mL in comparison with the respective BDP not sterilised are reported.

Tab.1

BDP batch	HPLC purity (% content)	Limits	BDP sample		
			Not sterilised	4 mg/mL sterilised	40 mg/mL sterilised
1	beclomethasone 17-propionate	≤ 1.0%	----	----	----
	beclomethasone 21-propionate	≤ 1.0%	0.34	0.32	0.36
	Rrt 0.60	≤ 0.1%	----	0.26	----
	Rrt 0.75	≤ 0.1%	----	----	----
	Rrt 0.86	≤ 0.1%	----	----	----
	Rrt 1.06	≤ 0.1%	----	0.80	----
2	beclomethasone 17-propionate	≤ 1.0%	0.13	0.09	0.13
	beclomethasone 21-propionate	≤ 1.0%	----	0.06	0.08
	Rrt 0.60	≤ 0.1%	----	0.21	----
	Rrt 0.75	≤ 0.1%	----	----	----
	Rrt 0.86	≤ 0.1%	----	----	----
	Rrt 1.06	≤ 0.1%	----	0.47	----
3	beclomethasone 17-propionate	≤ 1.0%	----	----	----
	beclomethasone 21-propionate	≤ 1.0%	0.10	0.06	0.12
	Rrt 0.60	≤ 0.1%	----	0.21	----
	Rrt 0.75	≤ 0.1%	----	----	0.07
	Rrt 0.86	≤ 0.1%	----	----	0.06
	Rrt 1.06	≤ 0.1%	----	0.57	----

[0035] Sterilised 4mg/mL BDP samples show two different unknown impurities (Rrt 0.60 and Rrt 1.06) not found in the respective starting drug substance. The content of these impurities is respectively about 0.3% and 0.8%. In the samples 40mg/mL the content of these unknown impurities is below 0.05% (according to the international guideline CPMP/ICH/2737/99 "Note for guidance on impurities testing: impurities new drug substances" the reporting threshold for impurity to be identified and qualified is 0.1%). The content of the other known impurities is not significantly modified by the steam sterilisation process. This evidence is confirmed by data reported in tab. 2 where the purity profile of sterilised 40mg/mL BDP suspension, batches 4 and 5 (different experimental set), is comparable with the purity of the BDP starting drug substances.

Tab. 2

HPLC Purity (% content)	limits	40mg/ml BDP (batch 4)		40mg/ml BDP (batch 5)	
		Not sterilized	Sterilized	Not sterilized	Sterilized
beclomethasone	≤ 1.0%	----	----	----	----
beclomethasone 17-propionate	≤ 1.0%	----	----	----	----
beclomethasone 21-propionate	≤ 1.0%	0.13	0.12	----	----
Rrt 0.37	≤ 0.1 %	----	----	----	----
Rrt 0.62	≤ 0.1%	----	----	----	----
Rrt 1.06	≤ 0.1-%	----	----	----	----

[0036] The HPLC purity of formulations was determined on the formulation reported below:

- PG038/115 containing sterilised BDP batch 4
- PG038/119 containing not sterilised BDP batch 4
- PG038/116 containing sterilised BDP batch 5
- PG038/120 containing not sterilised BDP batch 5

[0037] The analyses was performed after the preparation (time zero T0) and after 50 days of storage at condition of 40°C 75% R.H.

[0038] As reported in table 3 and 4 the purity of formulations containing sterilised BDP is not significant different from the purity of formulations containing the respective not sterilised BDP. The impurity content determined at T0 is non significantly different from the content determined after 50 days of storage at condition of 40°C 75% R.H.

Tab. 3

		Formulations			
HPLC Purity (% content)	limits	PG038/115 (sterilised BDP 4)		PG038/119 (not sterilised BDP 4)	
		T0	50 days	T0	50 days
beclomethasone	≤ 1.0%	----	0.08	----	0.08
beclomethasone 17-propionate	≤ 1.0%	----	0.10	----	0.09
beclomethasone 21-propionate	≤ 1.0%	0.12	0.09	0.12	0.09
Rrt 0.37	≤ 0.5%	----	0.07	----	0.09
Rrt 0.62	≤ 0.5%	----	0.15	----	0.12
Rrt 1.06	≤ 0.5%	----	----	----	----

Tab. 4

		Formulations			
HPLC Purity (% content)	limits	PG038/116 (sterilised BDP 5)		PG038/120 (not sterilised BDP 5)	
		T0	50 days	T0	50 days
beclomethasone	≤ 1.0%	----	0.07	----	----
beclomethasone 17-propionate	≤ 1.0%	----	0.10	----	0.12
beclomethasone 21-propionate	≤ 1.0%	----	----	----	----
Rrt 0.37	≤ 0.5%	----	----	----	0.09
Rrt 0.62	≤ 0.5%	----	0.19	----	0.13
Rrt 1.06	≤ 0.5%	----	0.06	----	0.09

Water stability test of drug substance

[0039] Water stability test was performed on sterilised 40mg/mL BDP suspension and data were compared to not sterilised BDP. The analysed BDP batches were batch 4 and batch 5.

[0040] No substantial differences on crystal shape and size were found between sterilised samples and not.

Particle size distribution of drug substance

[0041] Particle size, x-axis, is expressed as volume equivalent diameter (d_v). According to this definition each irregular particle is assumed to be a sphere. Such sphere is so defined *equivalent sphere*. Such sphere and the irregular particle have the same volume, therefore the volume of the sphere is defined as *volume equivalent sphere*, and the

diameter of such *volume equivalent sphere* is defined as *volume equivalent diameter*. A log scale is reported.

[0042] The number of particles within each sizeclasses was reported on the y-axis.

[0043] The particle size distribution was determined on sterilised 40mg/mL aqueous BDP suspension. Two different batches of drug substances were investigated: batch 4 and batch 5. In addition the particle size distribution of the same batches sterilised in presence of two different concentration of NaCl (0.420 g/mL and 0.570 g/mL, referred to as NaCl (B) and NaCl (C) respectively) were performed. The particle size distribution of samples containing BDP batch 4 and BDP batch 5 are respectively reported in figure 1 and figure 2. Analyses of sterilised BDP were performed on the sample described in Example 2.

[0044] For each particle size distribution, the percentage of particles below 5 and 10 μm and the D[4,3] (equivalent volume mean diameter) were determined. D[4,3] value is an index of the particles mean diameter considering the equivalent volume and mass of the particle.

[0045] The results are reported respectively in table 5 for batch 4 and table 6 for batch 5.

Tab. 5

		BDP batch 4			
		not sterilised	sterilised	sterilised + NaCl (0.42 g/mL)	sterilised + NaCl (0.57 g/mL)
D[4.3]		2.80 μm	3.27 μm	3.79 μm	2.9 μm
Particle size	< 5 μm	90.66 %	81.54 %	74.91 %	87.09 %
	< 10 μm	99.48 %	98.91 %	98.77 %	98.99 %

Tab. 6

		BDP batch 5			
		not sterilised	sterilised	sterilised + NaCl (0.42 g/mL)	sterilised + NaCl (0.57 g/mL)
D[4.3]		2.73 μm	3.38 μm	3.75 μm	3.37 μm
Particle size	< 5 μm	92.05 %	81.33 %	76.60 %	80.63 %
	< 10 μm	99.98 %	98.19 %	97.47 %	98.67 %

[0046] As shown in figures 1 and 2 and confirmed by the value referring to D[4,3] (tables 5 and 6) the sterilisation process promoted a slight crystal growth of BDP. The D[4,3] value of sterilised BDP was about 0.6 micron greater than the not sterilised. The amount of particle with a mean diameter less than 5 micron (n.b. particle size below 5 micron is considered to be the respirable fraction) was respectively around 80% for sterilised BDP and 90% for the not sterilised BDP. The amount of particles with a mean diameter less than 10 micron was always greater than 98%. Contrary to what it is reported by O'Neill (US 3962430) a growth of crystal size to 300-400 micron, subsequent to the sterilisation process, was not observed. The presence of NaCl at the two concentration (pre-mixed in the BDP suspension to be sterilised) did not substantially affect the particle size. The particle size profile of sterilised samples containing BDP + NaCl or BDP alone were not significantly different. Only the curve of sterilised BDP+0.42 mg/mL of NaCl (fig. 1) was slightly shifted towards the right (increase crystal size) in comparison with the curve of the sterilised BDP.

Particle size distribution of drug product

[0047] Particle size distribution of each formulation was determined for comparison. The compared formulations had the same quali-quantitative composition of excipients (see tab. 9), but contained sterilised BDP or not sterilised BDP as reported in tab. 7.

Tab.7

Batch formulation	Batch BDP	Characteristic of the batch
PG038/115	4	Sterilised
PG038/116	5	Sterilised
PG038/119	4	Not sterilised
PG038/120	5	Not sterilised

[0048] Analyses were performed on the sample after 50 days of storage at 40°C 75% R.H. Figure 3 shows particle size distribution of formulations PG038/115(S) and PG038/119(NS) Figure 4 shows particle size distribution of formulations PG038/116(S) and PG038/120(NS).

[0049] The D[4,3]value and the percentage of particle with a d_v lower than 5 and 10 μm of each analysed samples are reported in table 8.

Tab. 8

		PG038/119 (not sterilised BDP 4)	PG038/115 (sterilised BDP 4)	PG038/120 (not sterilised BDP 5)	PG038/116 (sterilised BDP 5)
D [4.3]		3.24 μm	3.21 μm	3.41 μm	3.53 μm
Particle size	< 5 μm	83.76 %	81.79 %	81.65 %	78.48 %
	< 10 μm	99.13 %	98.62 %	98.64 %	97.85 %

[0050] The curve profiles of formulations containing sterilised BDP and the respective not sterilised BDP are not significantly different. The D[4.3] and the amount of particles with a diameter less than 5 μm , of all formulations, were not affected by the characteristic of the used BDP. The D[4.3] value of formulation containing sterilised BDP was the same of the formulation containing not sterilised BDP. The percentage of particle with a diameter less than 5 micron was comparable in both formulations.

[0051] Similar results have been obtained with formulations containing steam sterilised BDP: water mixtures in all investigated ratios (range 2.5:100 - 100:2), for example mixtures containing 400 mg BDP and 1 ml water or mixtures containing 4g BDP and 1 ml water or even mixtures containing 40g BDP and 1 ml water.

[0052] A slight crystal growth is observed in the sterilised samples of drug substance, but the diameter of particles remains always below 20-30micron and no particles are observed with a size around 300-400micron, contrary to what stated in US 3,962,430. A saturated solution of sodium chloride, used instead of water only, doesn't affect the crystal size, so that the particle size distribution of sterilised BDP is not significantly different from the particle size distribution of BDP sterilised in the presence of sodium chloride.

[0053] The particle size distribution of formulations containing sterilised BDP and non-sterilised BDP respectively, is comparable after 50 days in samples stored at stressed condition, and no significant differences were found between the different formulations.

[0054] It has also been found that micronized aqueous suspensions of glucocorticoids can be efficiently steam sterilised under the above conditions without any modification of the purity of the drug substance. This result was also unexpected after the teachings of WO 00/25746, which reports that BDP suspensions subjected to a steam sterilisation process undergo a remarkable degradation amounting to about 8-9% of the active ingredient.

[0055] The steam sterilization of glucocorticoids according to the present invention is, therefore, the simplest and most economic process to be used in industrial plants for the preparation of pharmaceutical formulations of glucocorticoids, in particular of BDP, for inhalation delivery.

[0056] The process for the sterilisation of glucocorticoid, and beclomethasone dipropionate in particular, developed with the present invention offers therefore, considerable economic advantages in the development of an industrial aseptic process for a sterile glucocorticoid manufacturing in a formulation suitable for pulmonary delivery.

[0057] The present invention shall be illustrated by means of the following examples which are not construed to be viewed as limiting the scope of the invention.

Materials and Methods	
Materials	
	Supplier
Beclomethasone dipropionate	Farmabios
Sorbitan laurate	IVI
Polysorbate 20	IVI
Cetostearyl alcohol	IVI Chimica
Sodium monohydrogen phosphate bihydrate	Fluka
Potassium dihydrogen phosphate	Fluka
Equipment	
Autoclave: De	Lama mod. VS/E
Stirrer:	IKA RW 20 DZM
Homogenizer:	IKA Ultra Turrax T 50
Particle size analyser:	Fritsch Analysette A22

EXAMPLE 1

Steam sterilisation of aqueous BDP suspension.

[0058] Two different concentrations, 4mg/mL and 40mg/mL were used. The steam sterilisation was performed in autoclave at 121°C 20'. Three different batches of BDP were used hereinafter referred to as batch 1, batch 2 and batch 3.

[0059] The HPLC purity of sterilised DBP was evaluated in comparison to the non-sterilised BDP.

[0060] Each batch has prepared as follows:

BDP (4 mg) was suspended in 1 mL of purified water
BDP (40 mg) was suspended in 1 mL of purified water.

EXAMPLE 2

Particle size distribution and water stability test of sterilised BDP

[0061] Particle size distribution and water stability test were performed on sterilised BDP and, for comparison with non-sterilised BDP. BDP was sterilised as aqueous 40mg/mL suspension. In addition aqueous 40mg/mL BDP suspensions containing 420mg/mL and 570mg/mL of NaCl were sterilised. In both cases the steam sterilisation was carried out at 121°C 20'.

[0062] Two different batches of BDP were used (batch 4 and batch 5), of each preparation.

BDP batch 4 and BDP batch 5: 120 mg of BDP was suspended in 3 mL of purified water.

BDP batch 4 + NaCl (B) and BDP batch 5 + Nacl(B): 120 mg of BDP and 1.26 g of NaCl were suspended in 3 mL of purified water

BDP batch 4 + Nacl(C) and BDP batch 5 + Nacl(C): 120 mg of BDP and 1.71 g of NaCl were suspended in 3 mL of purified water

[0063] The particle size distribution curves were obtained using a laser particle sizer "Fritsch Analysette 22".

EXAMPLE 3

Formulation for stability study

[0064] Formulations containing sterilised BDP were prepared using the BDP samples described in Example 2.

[0065] Formulation batch number and the characteristic of BDP are reported in tab.7.

[0066] Particle size distribution was determined after 50 days of storage. HPLC purity was evaluated immediately after the preparation and after 50 days of storage at 40°C 75% R.H.

[0067] The quali-quantitative composition of the formulation are reported in Tab. 9 .

Tab. 9

<i>Ingredient</i>	<i>Amount</i>
BDP	40 mg
Sorbitan laurate	20 mg
Polysorbate 20	100 mg
Sodium monohydrogen phosphate bihydrate	724 mg
Potassium dihydrogen phosphate	354 mg
Sodium chloride	420 mg
Purified water	Up to 100 mL

[0068] Following is an exemplary method for the preparation of the BDP formulation of Table 9, which was carried out in 3 distinct phases:

Phase 1

[0069] Sorbitan laurate (0.180 g) and polysorbate 20 (0.900 g) were added to 400 mL of purified water. Then 9 mL of sterilised aqueous BDP suspension, corresponding to a total amount of 360mg of BDP, was added.

Phase 2

[0070] Sodium monohydrogen phosphate bihydrate (6.516 g), potassium dihydrogen phosphate (3.186 g) and sodium chloride (3.78 g) were dissolved in 200 mL of purified water.

Phase 3 - Final formulation

[0071] The preparations of phase 1 and 2 were mixed and diluted to 900 mL with purified water

[0072] Each final formulation was packaged into a 200 mL brownish glass bottle.

[0073] The formulations were submitted to stability studies under the accelerated condition of 40°C 75% R.H.

[0074] Other formulations were prepared to confirm the applicability of the process of the present invention.

[0075] The quali-quantitative composition of other formulations which have been tested is reported in Tab. 10 and Tab. 11.

Tab. 10

<i>Ingredient</i>	<i>Amount</i>
BDP	40 mg
Sorbitan laurate	20 mg
Polysorbate 20	100 mg
Sodium chloride	900 mg
Purified water	Up to 100 mL

Tab. 11

<i>Ingredient</i>	<i>Amount</i>
BDP	40 mg
Sorbitan laurate	20 mg
Polysorbate 20	100 mg
Cetostearyl alcohol	130 mg
Sodium monohydrogen phosphate bihydrate	724 mg

Tab. 11 (continued)

<i>Ingredient</i>	<i>Amount</i>
Potassium dihydrogen phosphate	354 mg
Sodium chloride	420 mg
Purified water	Up to 100 mL

5

10 **Claims**

15

20

25

30

35

40

45

50

55

1. A process for the steam sterilization of glucocorticoids comprising heating a mixture of micronized glucocorticoid and water at a temperature ranging between 100 and 130° C for a time sufficient to sterilise the mixture with a minimum S.A.L. of 10^{-6} , the mixture being a mixture of glucocorticoid and water only.
2. A process according to Claim 1, wherein the glucocorticoid:water ratio is selected in a range between 3:100 to 10:100
3. A process according to Claims 1 or 2, wherein the glucocorticoid is beclomethasone.
4. A process according to Claim 3, wherein beclomethasone is in the form of beclomethasone dipropionate.
5. A process according to any of Claims 1 to 4, wherein sterilization is carried out at a temperature of 121°C for 20 minutes.

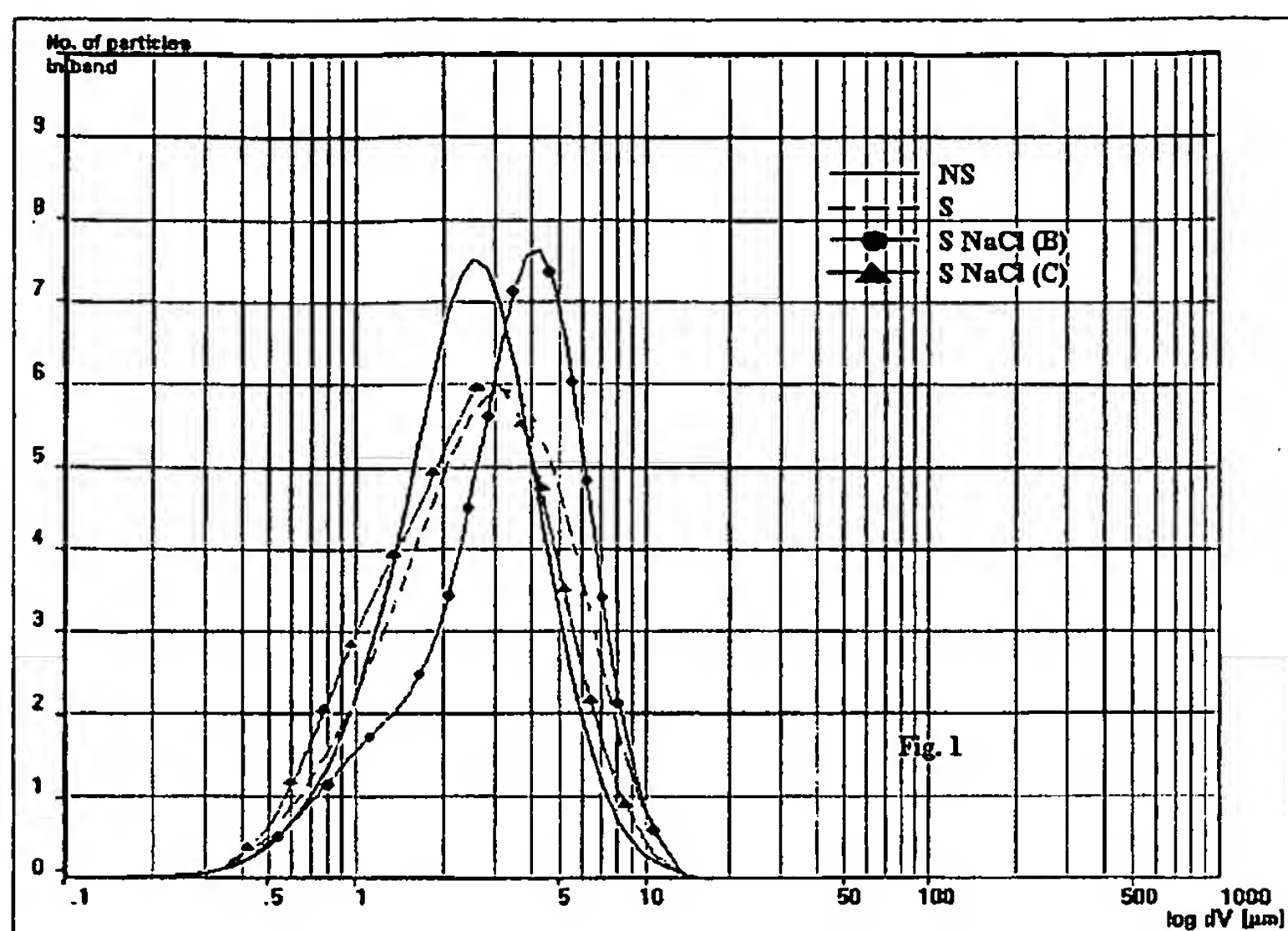


Fig. 1

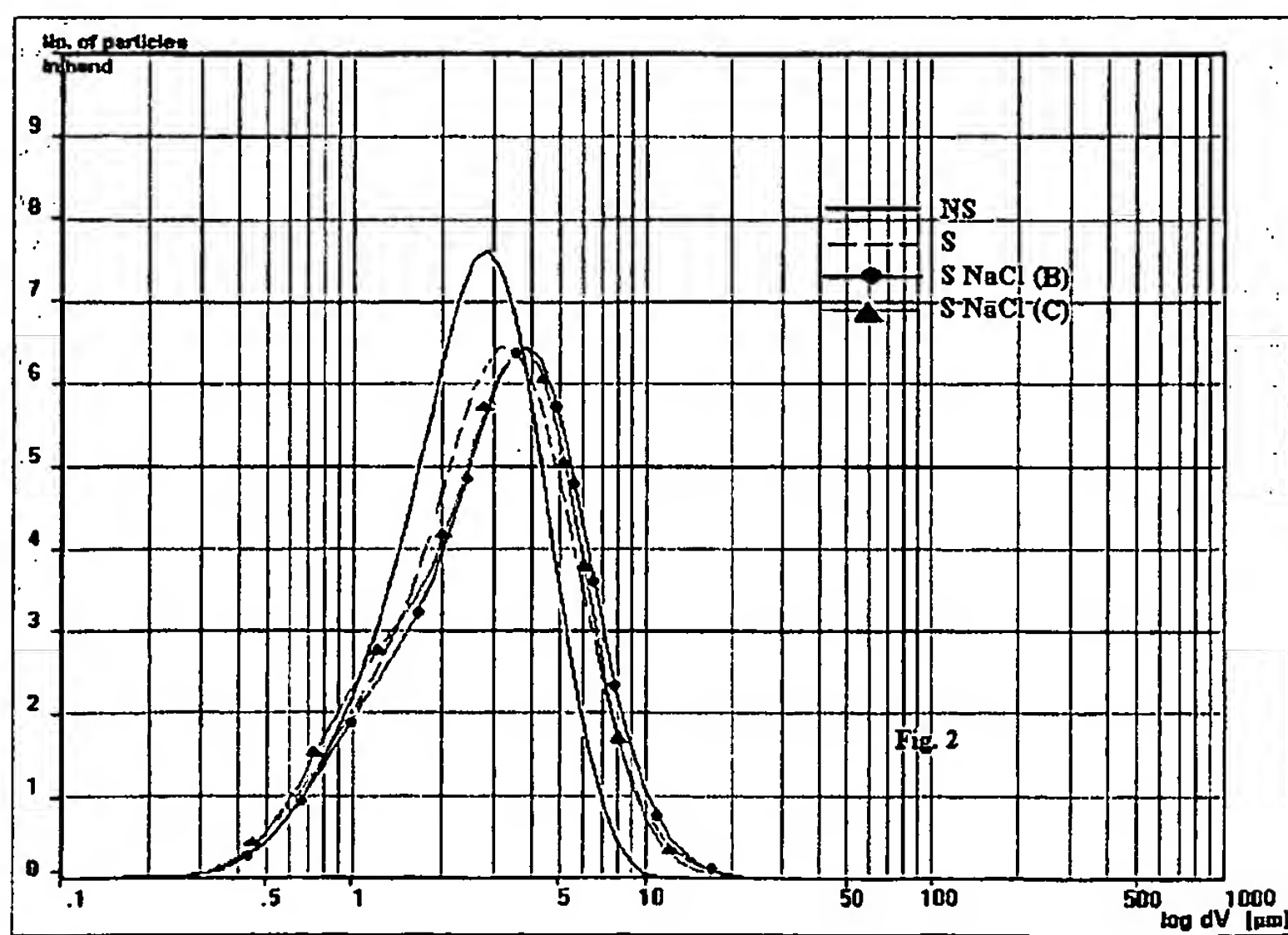


Fig. 2

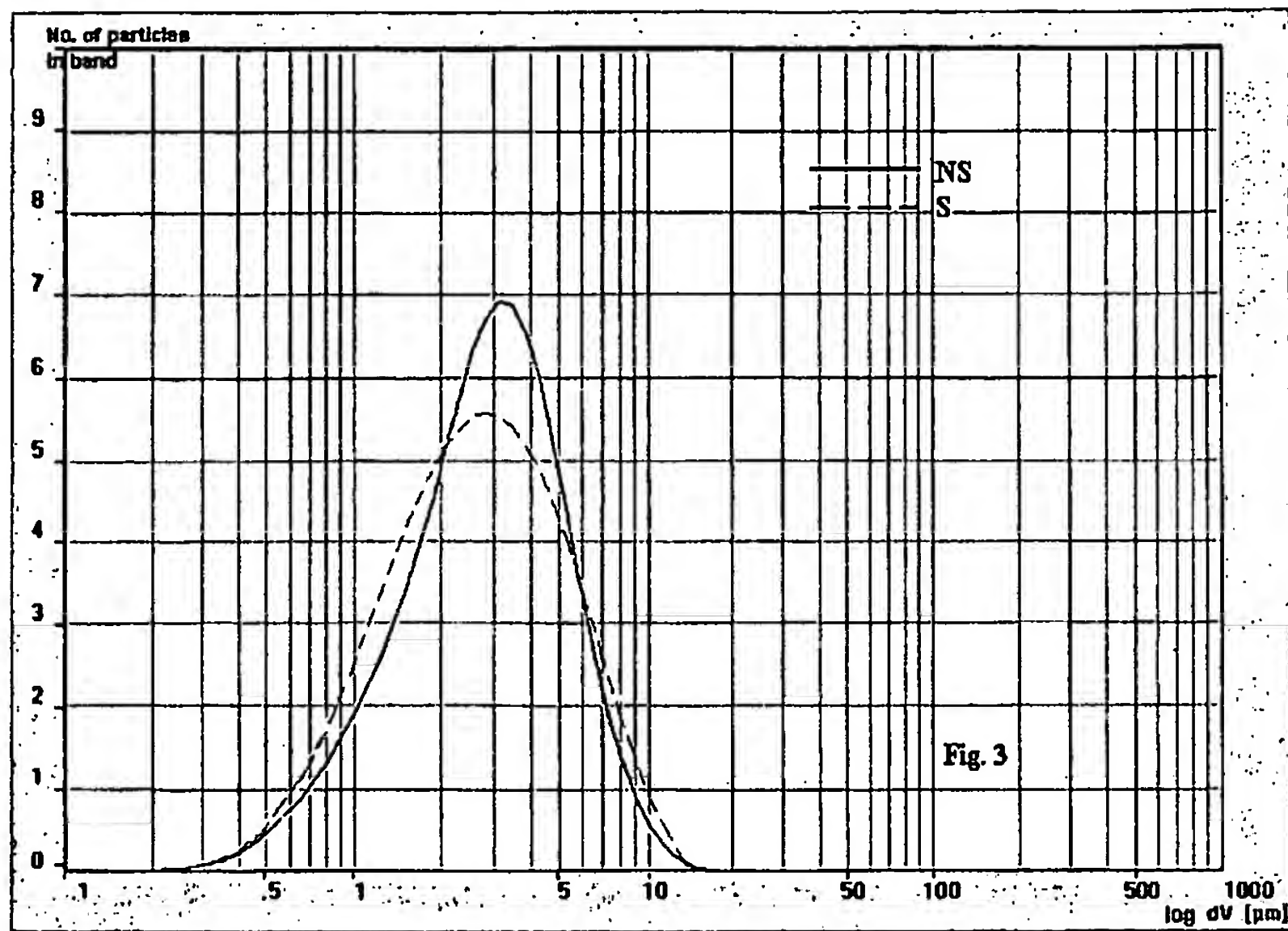


Fig. 3

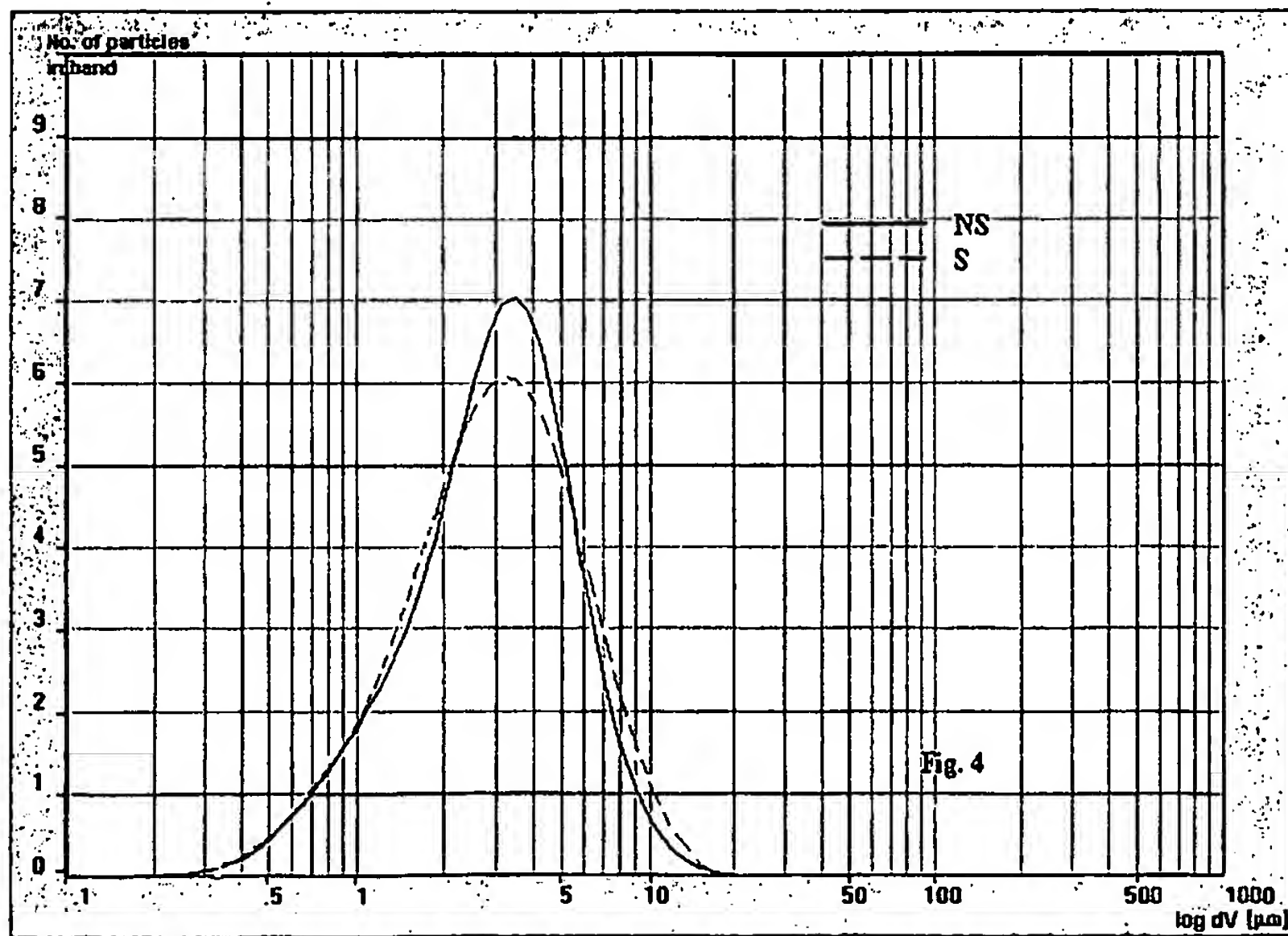


Fig. 4



European Patent
Office

EUROPEAN SEARCH REPORT

Application Number
EP 03 00 4726

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.7)
X,D	US 3 962 430 A (O'NEILL JOSEPH L) 8 June 1976 (1976-06-08) * column 2, line 1 - column 3, line 61; claims 1-5; examples 1-13,15,19-24 *	1,2,5	A61L2/07 A61K31/56 A61K31/57 A61K31/573 C07J5/00
X	WO 99 32156 A (BAYER AG) 1 July 1999 (1999-07-01) * page 5, line 16 - page 5, line 28 * * page 6, line 15 - page 6, line 25 * * page 10, line 10 - page 11, line 10; examples 1-8 *	1,2,5	C07J7/00 C07J51/00 C07J75/00
X	WO 95 31964 A (GLAXO WELLCOME AUSTRALIA LTD ;TAINSH DAVID ALEXANDER (GB); ILOTT T) 30 November 1995 (1995-11-30) * page 4, line 31 - page 5, line 2; examples 1,2 *	1,2,5	
X	WO 99 36055 A (NOVARTIS ERFIND VERWALT GMBH ;KIS GYOERGY LAJOS (CH); NOVARTIS AG) 22 July 1999 (1999-07-22) * page 6, paragraph SECOND - page 6, paragraph THIRD; example 4 *	1,2,5	
A	WO 02 41925 A (MCAFFER IAN GARDNER CAMERON ;BREATH LTD (GB); PUROHIT KAILASH SAJJ) 30 May 2002 (2002-05-30) * page 2, line 9 - page 8, line 7; example 2 *	1-5	TECHNICAL FIELDS SEARCHED (Int.Cl.7) A61L A61K C07J
A,D	WO 99 25359 A (MOLIN OVE ;ASTRA AB (SE); KARLSSON ANN KRISTIN (SE); LARRIVEE ELKI) 27 May 1999 (1999-05-27) * page 3, line 29 - page 7, line 23; examples 1-3,6,7 *	1-5	
The present search report has been drawn up for all claims			
Place of search MUNICH		Date of completion of the search 7 August 2003	Examiner Edmüller, P
<p>CATEGORY OF CITED DOCUMENTS</p> <p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document</p>			

EPO FORM 1503 (3.82 (P04C01))



European Patent
Office

EUROPEAN SEARCH REPORT

Application Number
EP 03 00 4726

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.7)
A, D	WO 00 25746 A (BRAMBILLA GAETANO ;BERNINI EVA (IT); CHIESI PAOLO (IT); MALVOLTI C) 11 May 2000 (2000-05-11) * example 1 * -----	1-5	
			TECHNICAL FIELDS SEARCHED (Int.Cl.7)
The present search report has been drawn up for all claims			
Place of search MUNICH		Date of completion of the search 7 August 2003	Examiner Edmueller, P
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document			

EPO FORM 1503 03.02 (P04/C01)

**ANNEX TO THE EUROPEAN SEARCH REPORT
ON EUROPEAN PATENT APPLICATION NO.**

EP 03 00 4726

This annex lists the patent family members relating to the patent documents cited in the above-mentioned European search report.
The members are as contained in the European Patent Office EDP file on
The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

07-08-2003

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
US 3962430	A	08-06-1976	NONE	
WO 9932156	A	01-07-1999	US 6066292 A	23-05-2000
			AU 730621 B2	08-03-2001
			AU 1630199 A	12-07-1999
			CA 2310698 A1	01-07-1999
			CN 1282256 T	31-01-2001
			EP 1039937 A2	04-10-2000
			JP 2001526089 T	18-12-2001
			WO 9932156 A2	01-07-1999
			ZA 9811621 A	23-06-1999
WO 9531964	A	30-11-1995	AT 207734 T	15-11-2001
			AU 710821 B2	30-09-1999
			AU 2614595 A	18-12-1995
			BR 9507746 A	19-08-1997
			CA 2190763 A1	30-11-1995
			CN 1148804 A ,B	30-04-1997
			CZ 9603423 A3	16-07-1997
			DE 69523587 D1	06-12-2001
			DE 69523587 T2	27-06-2002
			DK 760649 T3	28-01-2002
			WO 9531964 A1	30-11-1995
			EP 0760649 A1	12-03-1997
			ES 2164767 T3	01-03-2002
			FI 964634 A	20-11-1996
			HK 1004192 A1	12-04-2002
			HU 76552 A2	29-09-1997
			IL 113794 A	31-10-2000
			JP 10500420 T	13-01-1998
			NO 964938 A	20-11-1996
			NZ 287425 A	27-05-1998
			PL 317225 A1	17-03-1997
			PT 760649 T	29-04-2002
			RU 2161485 C2	10-01-2001
			SI 760649 T1	30-04-2002
			TW 438604 B	07-06-2001
			US 5993781 A	30-11-1999
			ZA 9504101 A	29-01-1996
WO 9936055	A	22-07-1999	EP 0938896 A1	01-09-1999
			AT 238036 T	15-05-2003
			AU 742920 B2	17-01-2002
			AU 2616999 A	02-08-1999
			CA 2315767 A1	22-07-1999
			DE 69907137 D1	28-05-2003

EPO FORM P0459

For more details about this annex : see Official Journal of the European Patent Office, No. 12/82

**ANNEX TO THE EUROPEAN SEARCH REPORT
ON EUROPEAN PATENT APPLICATION NO.**

EP 03 00 4726

This annex lists the patent family members relating to the patent documents cited in the above-mentioned European search report.
The members are as contained in the European Patent Office EDP file on
The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

07-08-2003

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
WO 9936055	A		DK 1047406 T3	21-07-2003
			WO 9936055 A1	22-07-1999
			EP 1172098 A1	16-01-2002
			EP 1047406 A1	02-11-2000
			JP 2002509101 T	26-03-2002
			US 2002165254 A1	07-11-2002
			US 6468548 B1	22-10-2002

WO 0241925	A	30-05-2002	AU 2389602 A	03-06-2002
			WO 0241925 A1	30-05-2002
			GB 2374013 A	09-10-2002
			US 2003103864 A1	05-06-2003

WO 9925359	A	27-05-1999	AU 744992 B2	07-03-2002
			AU 1266699 A	07-06-1999
			BR 9814118 A	03-10-2000
			CA 2310222 A1	27-05-1999
			CN 1285750 T	28-02-2001
			EP 1032396 A1	06-09-2000
			JP 2001523638 T	27-11-2001
			NO 20002470 A	05-07-2000
			NZ 504273 A	25-10-2002
			WO 9925359 A1	27-05-1999
			US 6392036 B1	21-05-2002
			US 2002065256 A1	30-05-2002
			ZA 9810217 A	14-05-1999

WO 0025746	A	11-05-2000	IT MI982364 A1	03-05-2000
			AU 762367 B2	26-06-2003
			AU 1266600 A	22-05-2000
			BR 9915251 A	30-10-2001
			CA 2349268 A1	11-05-2000
			CN 1335766 T	13-02-2002
			CZ 20011541 A3	12-09-2001
			WO 0025746 A2	11-05-2000
			EP 1126823 A2	29-08-2001
			HU 0104230 A2	28-03-2002
			JP 2002528484 T	03-09-2002
			NO 20012175 A	02-07-2001
			NZ 511305 A	25-07-2003
			PL 347908 A1	22-04-2002
			SK 5932001 A3	06-11-2001
			TR 200101209 T2	21-09-2001
			US 6464958 B1	15-10-2002

EPO FORM P0459

For more details about this annex : see Official Journal of the European Patent Office, No. 12/82